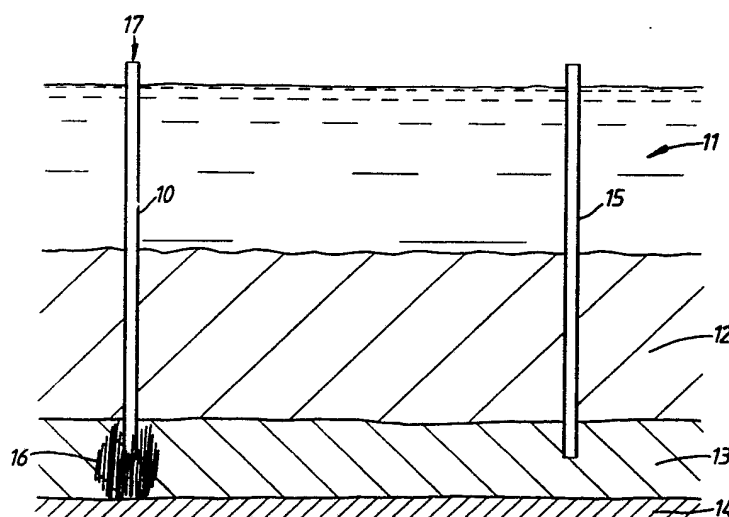




INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁵ : E21B 43/22	A1	(11) International Publication Number: WO 92/13172 (43) International Publication Date: 6 August 1992 (06.08.92)
(21) International Application Number: PCT/NO92/00016 (22) International Filing Date: 27 January 1992 (27.01.92) (30) Priority data: 9101840.8 29 January 1991 (29.01.91) GB (71) Applicant: DEN NORSKE STATS OLJESELSKAP A.S [NO/NO]; Postboks 300, Forus, N-4001 Stavanger (NO). (72) Inventor: SUNDE, Egil ; Draugveien 30, N-4300 Sandnes (NO). (74) Agent: LORENTZEN, Geir, B.; Den norske stats oljesels- kap a.s, Postboks 300, Forus, N-4001 Stavanger (NO).		(81) Designated States: AU, BR, CA, DK, NL, NO, RU Published <i>With international search report.</i>

(54) Title: METHOD OF MICROBIAL ENHANCED OIL RECOVERY



(57) Abstract

A method of microbial enhanced oil recovery for recovering oil from an oil-bearing rock formation (13). A population of aerobic bacteria (16) is introduced into the formation (13) at a position spaced from a production borehole (15). The microorganisms are adapted to use oil as a carbon source. Pressurised injection water (17) is introduced into the formation via an injection borehole (10), the water including a source of oxygen and mineral nutrients. The bacteria (16) multiply using the oil as their main carbon source and the oxygen in the injection water as their main oxygen source. In so doing, they dissociate the oil from the rock formation (15) and the dissociated oil is removed via the production borehole (15) by the injection water.

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AT	Austria	FI	Finland	MI	Mali
AU	Australia	FR	France	MN	Mongolia
BB	Barbados	GA	Gabon	MR	Mauritania
BE	Belgium	GB	United Kingdom	MW	Malawi
BF	Burkina Faso	GN	Guinea	NL	Netherlands
BG	Bulgaria	GR	Greece	NO	Norway
BJ	Benin	HU	Hungary	PL	Poland
BR	Brazil	IE	Ireland	RO	Romania
CA	Canada	IT	Italy	RU	Russian Federation
CF	Central African Republic	JP	Japan	SD	Sudan
CG	Congo	KP	Democratic People's Republic of Korea	SE	Sweden
CH	Switzerland	KR	Republic of Korea	SN	Senegal
CI	Côte d'Ivoire	LI	Liechtenstein	SU	Soviet Union
CM	Cameroon	LK	Sri Lanka	TD	Chad
CS	Czechoslovakia	LU	Luxembourg	TG	Togo
DE	Germany	MC	Monaco	US	United States of America
DK	Denmark	MG	Madagascar		
ES	Spain				

METHOD OF MICROBIAL ENHANCED OIL RECOVERY

The present invention relates to a method of microbial enhanced oil recovery.

When oil is present in subterranean rock formations such as sandstone or chalk, it can generally be exploited by drilling into the oil-bearing measures and allowing existing overpressures to force the oil up the borehole. This is known as primary removal. When the overpressure approaches depletion, it is customary to create an overpressure, for example by injecting water into the formations to flush out standing oil. This is known as secondary removal.

However, even after secondary removal, a great deal of oil remains in the formations; in the case of North Sea oil, this may represent 65% to 75% of the original oil present. Of this remaining oil probably more than half will be in the form of droplets and channels adhering to the rock formations that have been water-flooded and the remainder will be in pockets which are cut off from the outlets from the field. The present invention is concerned with the exploitation of the accessible but adhering oil remaining in the rock formations.

A number of enhanced oil recovery methods have been proposed, to address this objective. One approach is to combine pressure with a change in viscosity of the oil and/or water present. Thus, a diluent or CO₂ or steam is added to the reservoir to reduce the viscosity of the oil, thereby allowing it to be freed. Alternatively, viscosity-increasing additions such as polymers may be added to the injection water so that

the oil is preferentially dislodged. However, the application of CO_2 is disadvantageous due to scale formation, the use of steam is only effective in shallow reservoirs of low temperature while the other additives are very costly.

Another approach is to alter the surface tension and capillary forces so that the water under pressure is more accessible to the pores and channels. This may be achieved by alkaline flooding or by means of surfactants. However, these approaches also tend to be costly.

Another approach is in situ combustion. This entails pumping air or oxygen into the formation and igniting the gas/oil present. In theory, the heat produced will mobilise the lighter fractions as a combustion front moves steadily through the formation, with the heavier tars burning. In practice, however, it is almost impossible to control the progress since the gases tend to rise while the water present sinks, resulting in an uneven combustion front.

A fourth approach is microbial enhanced oil recovery (MEOR). This entails the use of micro-organisms such as bacteria to dislodge the oil, and a number of systems have been proposed. In the case of unconsolidated measures, such as oil shales, the oil bearing rock may be pumped as an aqueous slurry to surface settling tanks or resevoirs where it is subjected to aerobic bacteria, as disclosed in US 2907389. The availability of oxygen allows the bacteria to multiply, using the oil as a carbon source. In so doing, the bacteria produce surfactants which act to free the oil as droplets. The droplets of oil are less dense than water and so float to the surface. The

oil is then removed. Unfortunately, the system cannot conveniently be applied to consolidated rock formations, particularly when they are undersea.

In situ MEOR methods generally fall into two categories, aerobic bacteria systems, as described typically in US 3332487 and anaerobic bacteria systems as described in WO 89/10463.

The very existence of oil in a formation means that there cannot be present any anaerobic bacteria which will feed on oil under the prevailing conditions. Thus, in anaerobic bacteria systems, a source of carbon or "food" must be supplied. However, the bacteria selected (either deliberately or naturally) will be those most suited under the prevailing conditions to the consumption of the particular food employed. They will not be specifically adapted to have an effect on oil and therefore their action on oil will be as it were a by-product. Anaerobic systems therefore tend to be very slow in achieving the desired liberation of oil.

The absence of any oxygen in oil bearing formations means that if an aerobic system is to be used, then oxygen must be supplied. However, when aerobic bacteria are used and oxygen (or air, containing oxygen) is injected into the formation, the situation is far from satisfactory. Firstly, there is an immediate separation into a gaseous and an aqueous phase, which makes control of the system very difficult and in practice, limits the system to a batch-type operation. Secondly, a great deal of heat is generated, which, in view of the oxygen-rich gaseous phase and the readily available combustible material, presents a considerable risk of explosion. A cooling

medium must therefore also be employed.

It is therefore an object of the present invention to provide a method of MEOR which enables residual oil to be recovered more rapidly than is possible with anaerobic systems but without the risk of explosion.

It is a further object of the invention to provide such a method which can be readily controlled and which will be continuous, that is to say, after initiation in a particular zone, the process will proceed until substantially all the oil is recovered, without the need to re-treat the zone.

According to the invention, there is provided a method of microbial enhanced oil recovery for recovering oil from an oil-bearing second rock formation, the formation including an inlet at a first location and an outlet at a second location, the method comprising: injecting water containing a source of oxygen, capable of yielding at least 5mg/l free oxygen, into the formation at the first location spaced apart from the second location, allowing micro-organisms, which are either already present in the formation or which are introduced simultaneously with the oxygen containing injection water to multiply using the oil as their main carbon source and the oxygen from the injection water as their main oxygen source thereby establishing a biomass layer which acts to dissociate the oil from the rock formation, the dissociated oil then being removed via the outlet by the injection water.

In this system, on the far side of the injection well, the oxygen becomes the growth limiting factor due to the consumption of oxygen by the micro-organisms. The rate of growth of micro-organisms is of course

dependent on the available oxygen. In general maximum growth is desired and therefore it is desirable to maintain a high oxygen concentration in the injection water (and clearly also in advancing biomass layer). In some situations, where for instance it is desirable to stimulate the production of surfactants, level of oxygen in the water phase might be reduced in order to stress the micro-organisms into producing surfactants. This is at least one useful purpose in being able to adjust the oxygen concentration in the injection water.

A situation can then be established in which the biomass layer forms a front between the oxygen-rich injection water and oxygen-depleted water on the outlet side of the front. Initially, the oxygen-depleted water will be the formation water or oxygen free injection water but as the process progresses, it will be displaced by injection water, stripped of its oxygen as it passes through the biomass layer. Where the biomass is in contact with oil and has access to oxygen, it will feed on the oil, thereby dissociating the oil from the rock by one or more of a number of mechanisms. The principal mechanism is believed to be the production of surfactants which reduce the forces attaching the oil to the rock. The pressure of the injection water then forces the oil out of the rock pores and the oil is carried forwards by the injection water.

The oxygen is all consumed by the biomass, thus maintaining the front as the injection water passes through. Any oil degrading micro-organisms that are washed out by the water will become dormant due to the lack of oxygen. As the displaced oil is washed forwards, the micro-organisms at the rear of the front

will have no oil and will either become dormant or will feed on each other. This effectively regulates the thickness of the biomass layer ensuring that the oxygen penetrates to the forward part of the layer, allowing fresh oil to be acted upon. Thus, the front advances through the oil towards the outlet and dislodged oil is constantly being flushed out by the injection water.

By a process of natural selection, only the most successful micro-organisms thrive and these will be the ones most effective in using the oil. They will therefore be the most efficient at dislodging the oil, probably by the production of surfactants. However, due to the flushing action of the injection water, the displaced oil is removed and so only a very small proportion of the oil will actually be consumed by the biomass.

One theory as to how the oil is dissociated is that the oil is split into small droplets by the surfactants and these are washed out. However, the present applicants believe that the oil is initially disposed in long strands or ribbons in the rock pore structure and that the surfactants begin to effect only portions of these strands. In this way, the overall viscous forces attaching a strand will be reduced and the injection water pressure eventually dislodges the entire strand, rather than its being broken up by the surfactants.

The micro-organisms may be any convenient single-cell organisms such as yeasts but are most preferably bacteria. Suitable bacteria may be Pseudomonas putida, Pseudomonas aeruginosa, Corynebacterium lepus, Mycobacterium rhodochrous, Mycobacterium vaccae, Acinetobacter and Nocardia. The bacteria used may be

pre-selected and cultivated to thrive in the injection water under the prevailing conditions.

The oxygen in the injection water is preferably present as dissolved gas, though conceivably, it may be present as some other known oxidising agent either in solution or suspension. Suitable oxidising agents might be H_2O_2 , NaClO_3 , KClO_4 , NaNO_3 . Since the pressures involved with the injection water are necessarily very high to enable the water to be injected, the amount of gaseous oxygen that can be dissolved is quite considerable. The pressures encountered in the oil-bearing formations may be from 200 to 800 bar (20-80 MPa); at these pressures up to 4.0g of oxygen may be dissolved in a litre of water. This quantity is amply sufficient to allow aerobic bacteria to multiply at a satisfactory rate with a bulk flow rate of the injection water which is low enough to avoid reservoir damage.

Preferably, therefore, the amount of oxygen dissolved will be from 1mg/l to 4000mg/l more preferably from 40mg/l to 400mg/l though the actual amount will be dependent upon the prevailing conditions. The amount of oxygen present should not be so much as would be toxic to the bacteria.

The micro-organisms will in all probability produce CO_2 as they multiply. However when dissolved oxygen in the injection water is used, the volume of CO_2 produced will be in a 1:1 molar ratio with the oxygen consumed and will therefore enter into solution, particularly since its solubility is much higher than that of oxygen. More CO_2 than indicated by this ratio may be produced by other reactions, in which oxygen is taken from other sources, e.g. water, once

the bio degradation of hydro-carbon molecules has been initiated. Even where an oxidising agent is used, the solubility of CO_2 will be sufficient to avoid phase separation. The CO_2 produced will have a beneficial effect on the recovery of oil from the formation.

In practice, the avoidance of a gas phase is very important since microbial activity can only proceed in the liquid phase. Clearly, if a gas phase is present, the oil adhering to the rock formation within the gas phase will remain unaffected by the micro-organisms.

While many nutrient requirements of the micro-organisms may be met by the minerals naturally present, the injection water may have added to it essential nutrients, in particular to provide a source of nitrogen and phosphates. Examples of nutrient additives include NaNO_3 , KNO_3 , NH_4NO_3 , Na_2HPO_4 , K_2HPO_4 , NH_4Cl .

It will be appreciated that by using a system according to the invention, the advancing biomass layer will remove effectively all the oil it encounters. Either the oil will be dislodged and flushed away or it will be consumed and converted since any oil not dislodged will remain in the oxygen-rich side. Thus, a single continuous operation should be sufficient to treat a particular zone. The liberated oil can be separated from the water, minerals and organic material by conventional methods though it is desirable to minimise any pre-separation exposure to air in order to avoid further microbial action on the oil.

When the formation is depleted there is no need for further operations of the kind indicated - the production zone will be shut down.

The invention may be carried into practice in

various ways and an embodiment will now be described by way of example with reference to the accompanying drawings in which:-

Figure 1 is a schematic vertical section showing the initiation of a method according to the invention in a residual oil-bearing formation; and

Figures 2 to 4 are similar simplified views showing sequential steps in the process.

The invention will also be illustrated with reference to a laboratory scale, controlled test procedure carried out by Terje Torsvik, Roald Nilsen and Janiche Beeder, all of the Dept. of Microbiology and Plant Physiology, University of Bergen.

Figure 1 shows an undersea oil well which has been subjected to primary/secondary removal by means of an injection well 10. Beneath the sea 11 there are various core strata 12, a residual oil bearing formation 13 and an underling bed rock 14. A producing borehole 15 and the injection borehole 10 extend into the formation 13. In the case of a North Sea oilfield such as the Gullfaks field, the formation 13 might be consolidated sandstone which has a large quantity of adhering oil and which is flooded with formation and injection water containing no oxygen.

Injection water 17 is introduced into the formation 13 via the injection well 10. If there are no aerobic bacteria present in the formation 13 either naturally or due to operations carried out previously aerobic bacteria will be introduced via the injection well 10 e.g. with the injection water 17. The injection water 17 is rich in oxygen and various mineral nutrients such as ammonia and phosphates.

When the oxygen-rich injection water 17, the

bacteria and the oil come into mutual contact, the bacteria attacks the oil, and multiplies, creating biofilm 16 converting some of the oil to lighter fractions and producing surface active agents or surfactants. The production well 15 will act as a sink and there will be an overall flow of bioorganic matter (biofilm) produced by the micro-organisms, oil and injection/formation water from the injection well 10 towards the production well 15.

The injection water 17 is moving through the formation 13 towards the borehole 15 at a speed of about 0.1-15m/day carrying the formation/injection water before it. The formation water is removed via the borehole 15. The surfactants produced by the biofilm 16 help to reduce the forces by which the oil is attached to the rock formation and so the flowing injection water 17 actually detaches the oil 18 and this is carried forward through the formation 15.

As the injection water 17 passes through the biofilm 16, the oxygen is consumed by the multiplying bacteria. A steady state is reached when the thickness of the bacteria layer is such that no oxygen escapes the forward end. At this stage, the bacteria at the forward end of the layer receive less oxygen than the bacteria at the rear and so multiply more slowly. However, the bacteria at the rear run out of food (oil) and so they die. This tends to reduce the thickness of the layer and so more oxygen reaches the forward layers enabling the bacteria there to multiply. In this way, the bacteria layer moves steadily through the formation 13 at a rate of about 0.1 to 15m/day. The oxygen is thus the controlling factor of the bacterial action. Any oil-degrading bacteria which is washed out by the

injection water will cease to be active once it has left the bacteria layer since there will be no available oxygen.

As shown in Figure 3, the detached oil 18 flows out into the borehole 15 with the injection water. This is recovered at the surface and separation is carried out in a known manner.

Eventually, the biofilm 16 reaches the borehole 15 and the well is shut down as shown in Figure 4. The formation 13 will then be depleted of the oil previously adhering there.

While Figures 1 to 3 show the effect of the invention in one dimension, it will be appreciated that in practice, the situation would be a good deal more complex. In particular, the bacteria 16 would be arranged to converge on the borehole 15 from many or all directions, as depicted schematically in Figure 4. Furthermore, there would probably be a number of boreholes, which would be in use simultaneously.

After removal of the bacteria 16, the well 15 would be shut down.

The described method is not in any way was restricted to tertiary oil recovery. It can be used simultaneously to the injection of water in secondary oil recovery, as well as at the start of production of an oil field if and when the injection of water is found feasible. As will be evident to those skilled in the art, the use of water injection optionally in combination with this method will depend on the chosen strategy for producing hydrocarbons from a certain oil field.

Test Example I

A Hopeman sandstone core measuring 5x45cm containing residual oil after water flooding was used. The core had the following specification:-

Volume	884 cm ³
Pore Volume	166 cm ³
Permeability	700 mD
Residual oil	61 cm ³
Wettability	water wet

Injection water, including bacterial inocula comprising a mixed population of aerobic oil degraders grown at 45°C, was passed through the core at a nominal pressure of 2 bar and at a superficial velocity of 0.5m per day. The temperature was maintained at 45°C. The composition of the injection water was as follows:-

K ₂ HPO ₄	1.0 g/l
NH ₄ Cl	0.25 g/l
NaCl	20.0 g/l
MgCl ₂ *6H ₂ O	3.0 g/l
KCl	0.5 g/l
CaCl ₂ *2H ₂ O	0.15 g/l
NaHCO ₃	1.8 g/l
5 ml/l vitamin solution	
1 ml/l trace element solution	
Oxygen 1mg/l	

Under these conditions, an additional 5.5cm^3 of oil were produced during the passing of 22 pore volume equivalents. This gives a ratio of 2.5cm^3 oil produced for each mg of oxygen injected which is an oxygen efficiency of 2500.

CLAIMS

1. A method of microbial enhanced oil recovery for recovering oil from an oil-bearing rock formation, the formation including an inlet at a first location and an outlet at a second location, the method comprising: injecting water containing a source of oxygen, capable of yielding at least 5mg/l free oxygen, into the formation at the first location spaced apart from the second location, allowing micro-organisms, which are either already present in the formation or which are introduced simultaneously with the oxygen containing injection water, to multiply using the oil as their main carbon source and the oxygen from the injection water as their main oxygen source thereby establishing a biomass layer which acts to dissociate the oil from the rock formation; and removing the dissociated oil from via the outlet by the injection water.

2. A method as claimed in Claim 1 in which the micro-organisms are bacteria.

3. A method as claimed in Claim 2 in which the bacteria substantially comprises oil degrading aerobic and facultative anaerobic bacteria.

4. A method as claimed in Claim 3 in which the bacteria substantially comprises species of the genres of Pseudomonas putida, Pseudomonas aeruginosa, Corynebacterium lepus, Mycobacterium rhodochrous, Mycobacterium vaccae, Acinetobacter or Nocardia.

5. A method as claimed in any preceding Claim in which the source of oxygen in the injection water is dissolved gaseous oxygen.

6. A method as claimed in any of Claims 1 to 4 in which the source of oxygen in the injection water is provided by oxidising compounds such as H_2O_2 , $NaClO_3$, $KClO_4$ or $NaNO_3$, optionally in combination with dissolved gaseous oxygen.

7. A method as claimed in Claim 5 or Claim 6 in which the concentration of oxygen is between 1mg/l and 4000mg/l.

8. A method as claimed in any preceding Claim in which the oxygen concentration is below a level which is toxic to the micro-organisms.

9. A method as claimed in any preceding Claim in which the injection water also includes mineral nutrients.

10. A method as claimed in Claim 9 in which the mineral nutrients include a source of nitrogen and a source of phosphates.

11. A method as claimed in any preceding Claim in which the superficial velocity of the injection water through the oil-bearing formation is between 0.1 and 15m/ day.

12. A method as claimed in any preceding Claim in which the microorganisms produce surfactants which act

to dislodge the oil.

13. A method as claimed in Claim 12 in which the supply of oxygen and any nutrients in the injection water is intermittently substantially reduced in order to induce the production of surfactants by the micro-organisms.

14. A method as claimed in Claim 13 in which the reduction is carried out for periods of 5 to 50 hours.

15. A method as claimed in any preceding Claim applied to more than one outlet from the oil-bearing formation.

16. A method as claimed in any preceding Claim in which the outlet is a borehole.

17. A method of microbial enhanced oil recovery substantially as herein described with reference to and as shown in the accompanying drawings.

1/1

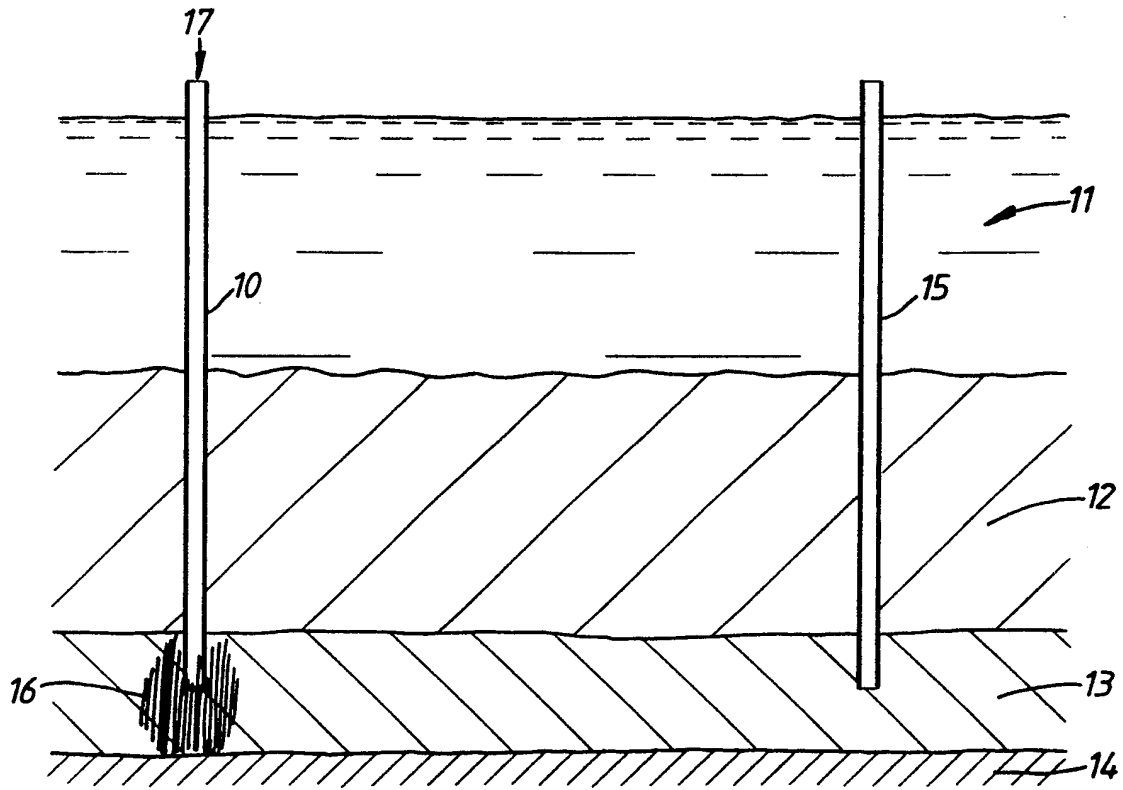


Fig. 1. v

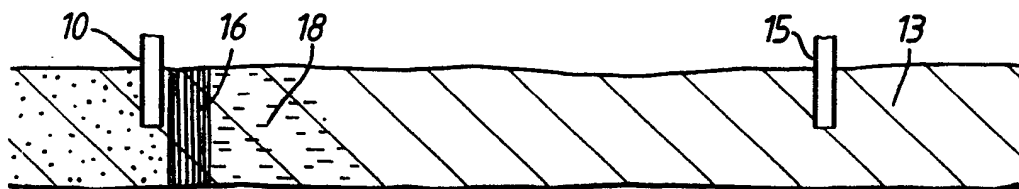


Fig. 2.

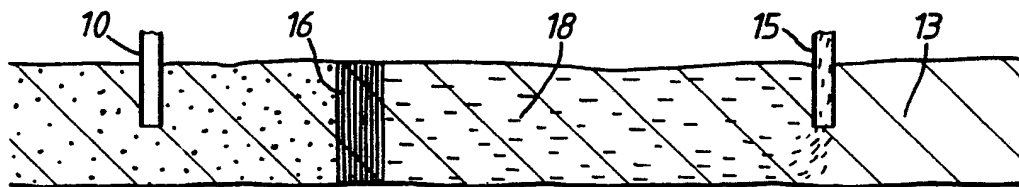


Fig. 3.

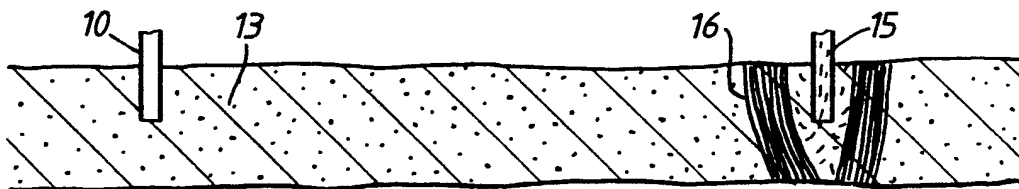



Fig. 4.

INTERNATIONAL SEARCH REPORT

International Application No PCT/NO 92/00016

I. CLASSIFICATION OF SUBJECT MATTER (If several classification symbols apply, indicate all) ⁶		
According to International Patent Classification (IPC) or to both National Classification and IPC		
IPC5: E 21 B 43/22		
II. FIELDS SEARCHED		
Minimum Documentation Searched ⁷		
Classification System	Classification Symbols	
IPC5	E 21 B	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in Fields Searched ⁸		
SE,DK,FI,NO classes as above		
III. DOCUMENTS CONSIDERED TO BE RELEVANT⁹		
Category *	Citation of Document, ¹¹ with indication, where appropriate, of the relevant passages ¹²	Relevant to Claim No. ¹³
Y	US, A, 4349633 (H.E. WORNE ET AL) 14 September 1982, see column 1-4, line 34 and the claims --	1-4, 12
Y	US, A, 3332487 (W.J. LOYD) 25 July 1967, see column 1 - column 4 -- -----	1-4, 12
<p>* Special categories of cited documents: ¹⁰</p> <p>"A" document defining the general state of the art which is not considered to be of particular relevance</p> <p>"E" earlier document but published on or after the international filing date</p> <p>"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)</p> <p>"O" document referring to an oral disclosure, use, exhibition or other means</p> <p>"P" document published prior to the international filing date but later than the priority date claimed</p> <p>"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>"X" document of particular relevance, the claimed invention cannot be considered novel or cannot be considered to involve an inventive step</p> <p>"Y" document of particular relevance, the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.</p> <p>"&" document member of the same patent family</p>		
IV. CERTIFICATION		
Date of the Actual Completion of the International Search	Date of Mailing of this International Search Report	
24th April 1992	1992 -05- 06	
International Searching Authority	Signature of Authorized Officer	
SWEDISH PATENT OFFICE	 Christer Bäcknert	

FURTHER INFORMATION CONTINUED FROM THE SECOND SHEET

V. ☒ OBSERVATIONS WHERE CERTAIN CLAIMS WERE FOUND UNSEARCHABLE¹

This international search report has not been established in respect of certain claims under Article 17(2) (a) for the following reasons:

1. ☒ Claim numbers.....17...., because they relate to subject matter not required to be searched by this Authority, namely:

The claim is drawn in a way which is not allowed, according to PCT Rule 6.2(a).

2. ☐ Claim numbers....., because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:

3. ☐ Claim numbers....., because they are dependent claims and are not drafted in accordance with the second and third sentences of PCT Rule 6.4(a).

VI. ☐ OBSERVATIONS WHERE UNITY OF INVENTION IS LACKING²

This International Searching Authority found multiple inventions in this international application as follows:

1. ☐ As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims of the international application.
2. ☐ As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims of the international application for which fees were paid, specifically claims:
3. ☐ No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the the claims. It is covered by claim numbers:
4. ☐ As all searchable claims could be searched without effort justifying an additional fee, the International Searching Authority did not invite payment of any additional fee.

Remark on Protest

- ☐ The additional search fees were accompanied by applicant's protest.
- ☐ No protest accompanied the payment of additional search fees.

ANNEX TO THE INTERNATIONAL SEARCH REPORT ON INTERNATIONAL PATENT APPLICATION NO.PCT/NO 92/00016

This annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report.
The members are as contained in the Swedish Patent Office EDP file on **28/02/92**
The Swedish Patent Office is in no way liable for these particulars which are merely given for the purpose of information.

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
US-A- 4349633	82-09-14	CA-A- 1154701	83-10-04
US-A- 3332487	67-07-25	NONE	